

Supporting Information for:

**Electrolytic cement clinker production sustained through
orthogonalization of ion vectors**

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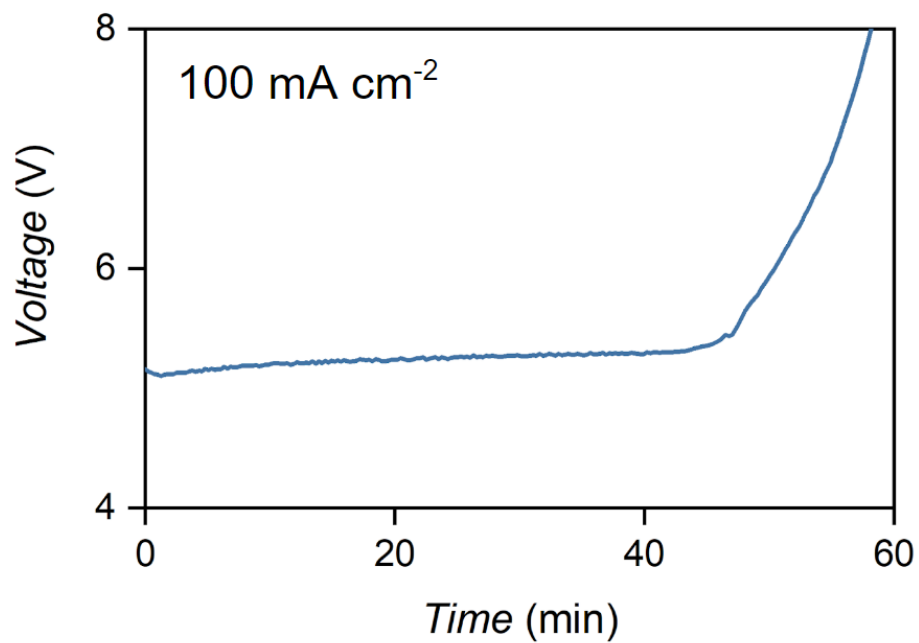


Figure S1. voltage-time characteristics of the cement electrolyser operating at 100 mA cm⁻². The cell voltage (V_{cell}) notably increases during electrolysis. The magnitude of the voltage increase varies between experiments, a representative voltage-time curve is shown here.

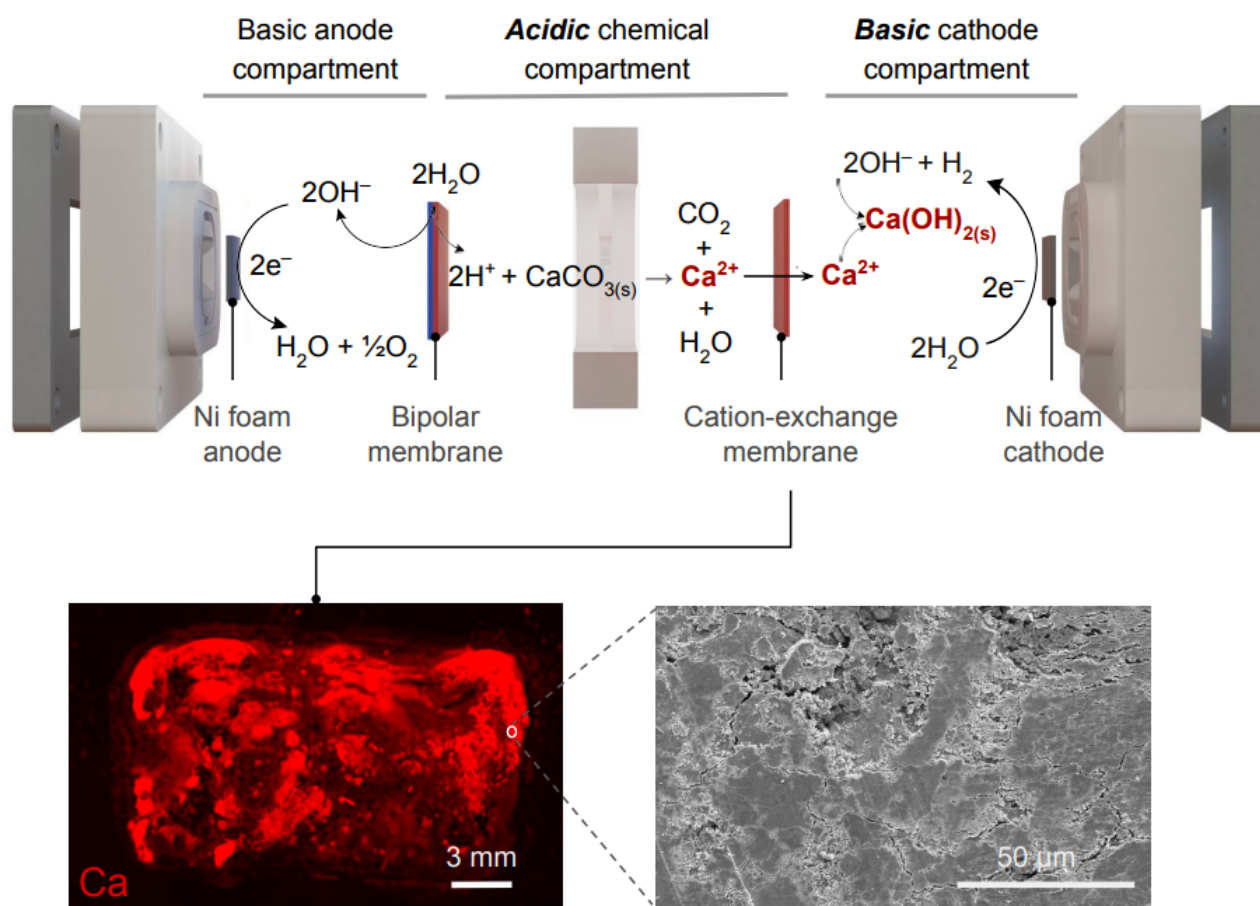


Figure S2. $\text{Ca(OH)}_{2(s)}$ deposition on the cation-exchange membrane during electrolysis. Expanded view of the flow electrolyser reported in our previous work which consists of anode, chemical, and cathode compartments. A BPM separates the anode and chemical compartments, and a CEM (Nafion 117) separates the chemical and cathode compartments. Nickel foam was used as both the anode and cathode. Bottom line: XRF and SEM images of a Nafion membrane before and after electrolysis at 100 mA cm^{-2} . Clusters of precipitated $\text{Ca(OH)}_{2(s)}$ are observed on the surface of Nafion after electrolysis.

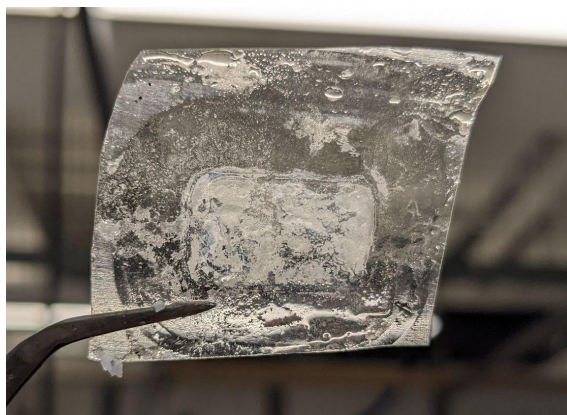


Figure S3. Optical photo of a Nafion 117 membrane after electrolysis. Noticeable $\text{Ca}(\text{OH})_2$ was found on its surface.

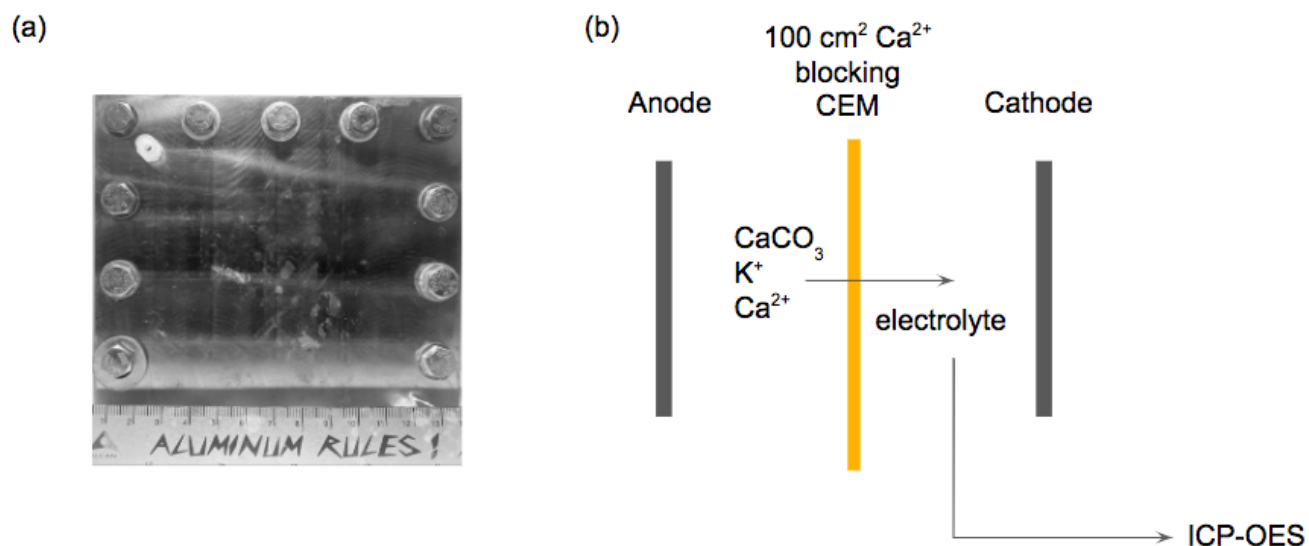


Figure S4. The optical photo of a $10 \times 10 \text{ cm}^2$ (active area) electrolyser. For the Ca^{2+} blocking selectivity test, 0.05 M CaCl_2 in 1 M KCl solution with excessive $\text{CaCO}_{3(s)}$ was fed into the anode, and the catholyte was collected every 30 min for ICP-OES test to determine the $[\text{Ca}^{2+}]$ for continuous 2 h.



Figure S5. The optical photo of the *operando* imaging system. The imaging system consisted of a modified two-compartment electrolyser with an open cathode compartment so we could image the CEM through the transparent catholyte with a high-resolution single-lens reflex (SLR) camera fixed above the electrolyser

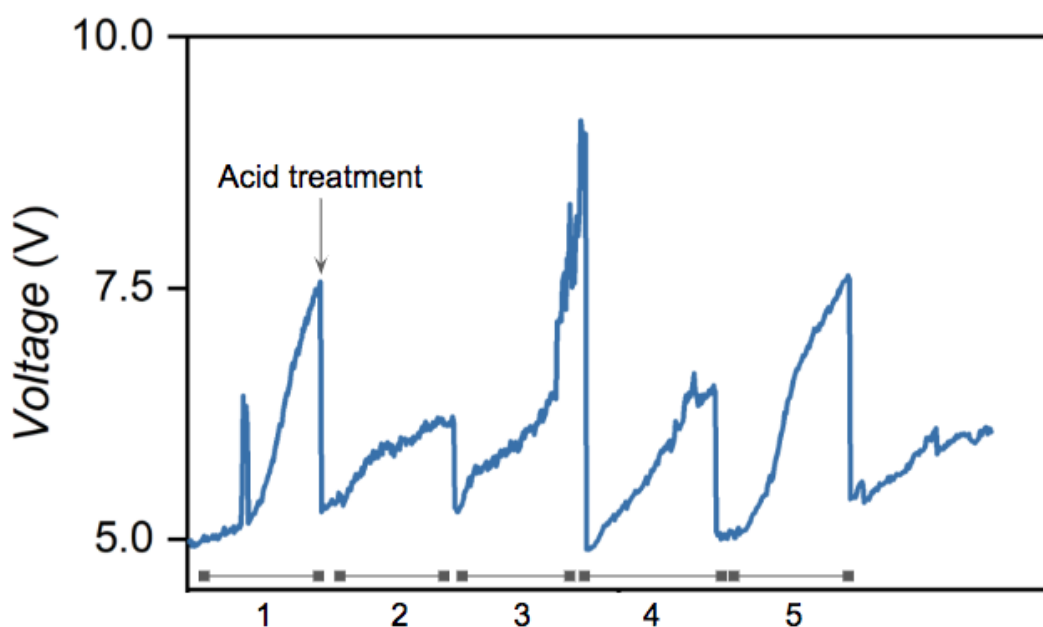


Figure S6. V_{cell} changes before and after acid treatment for the deposit removal. We performed cement electrolysis with a pristine Nafion 117 and we recorded V_{cell} with time. The electrolyser was stopped and the electrolyte at the cathode compartment was drained after a significant increase in V_{cell} . Then 1 M HCl was circulated to the cathode compartment to remove the $\text{Ca}(\text{OH})_{2(s)}$ on the Nafion (towards cathode). This acid treatment can bring V_{cell} to the original voltage for multiple cycles. This result proved the deposit effect is reversible.

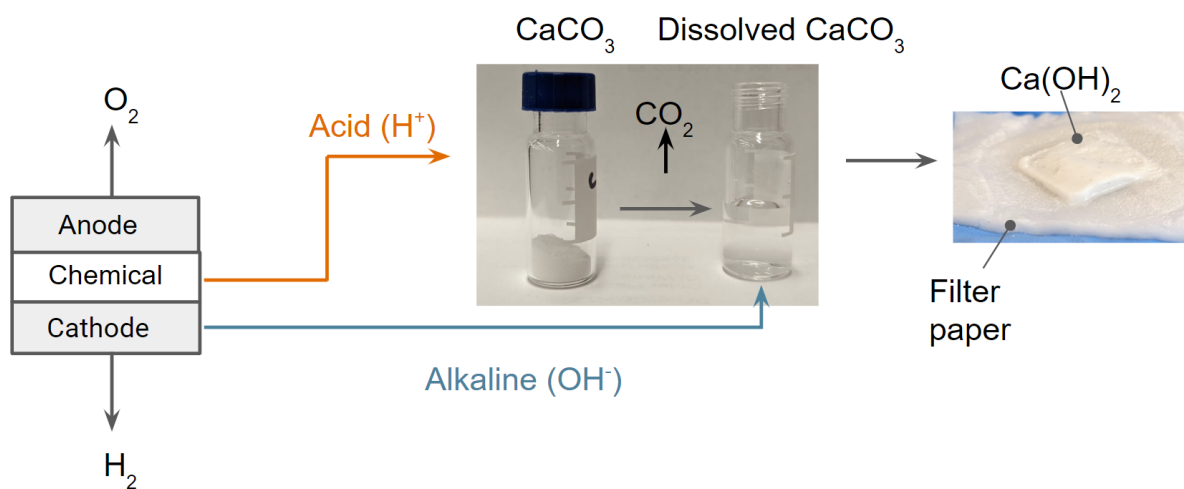


Figure S7. Electrochemical cement production using acid and base generated by an electrolyser. In this scenario, $\text{CaCO}_{3(s)}$ is not directly fed into electrolyser but reacts with the acid and base in sequence in a separated reactor - $\text{CaCO}_{3(s)}$ decomposes reacting with acids and releases Ca^{2+} , and it can be subsequently converted into $\text{Ca}(\text{OH})_{2(s)}$ with additional bases.